Yukon Zinc CORPORATION

Wolverine Project

MILL OPERATING PLAN

VERSION 2006-01

Prepared by:
Yukon Zinc Corporation

In Association with:
Hatch
Confidential Mineral Services

May 2006

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1 Introduction

This report was prepared by Yukon Zinc Corporation (YZC) with contributions from Confidential Mineral Services and Hatch. Confidential Mineral Services was responsible for the management and interpretation of laboratory tests and analyses of samples and recommended process design criteria. Hatch completed the process flowsheets based on the design criteria, selected equipment and prepared preliminary design drawings.

This report provides details pertaining to the daily and annual production rate, production schedule, general mill building layout, reagent use, concentrate haulage, power plant and fuel storage. Additional information on the infrastructure and processes for producing concentrates is contained within the *Wolverine Project Environmental Assessment Report* (YZC, 2005).

1.1 Mill Building

The mill building site was selected in order that the foundations could be keyed into the EXMT iron formation. This formation is the most competent of the local rocks, yet was found to be rippable in the exploration trench nearby. The ore processing facilities will be housed in a 136 m long x 36 m wide pre-engineered steel structure building covered with corrosion resistant metal cladding. Several modular structures will be provided along the northeast wall to serve as a main motor control center and mill shifters' offices. The crushing area will be located at the southeast corner of the building in a lean-to structure. Another lean-to structure will be built at the northwest corner to accommodate the air compressors, water treatment plant and reagent mixing area. The area in which the concentrate trucks will park for loading will also be constructed as a lean–to. It will have truck doors at each end and will contain an automated weighbridge. The industrial complex layout and sections are provided in Drawings A0-C-006, A0-C-010 and A0-C-011, and the mill building is shown in Drawings F1-G-001 through 003.

1.2 Production

1.2.1 Daily Production Rate

The project work to-date has assumed a milling rate of 1250 t/d.

A simple method of arriving at an indicative mining rate is Taylor's rule, an experienced appreciation of the constraints imposed by the ore body geometry and project economics, as follows:

$$\text{Daily Production Rate} = 0.014*(\text{reserves})^{0.75}$$

For a 5.2 Mt orebody, Taylor's rule yields a nominal mining rate of 1526 t/d.

The projected production rate for the mine is set at 1440 t/d of diluted ore, based on 1250 t/d of mill feed plus an additional 190 t/d of flotation rock from the DMS plant.

1.2.2 Annual Production Rate

Production will begin on the upper five stoping levels, from 1250 to 1330 m. This zone contains 1.6 Mt of ore and will provide almost the entire mill feed from startup to the year 2010. Mining will proceed down-dip on the orebody, developing a new level each year on average. In 2016, the mine will have achieved its ultimate depth of 1080 m elev. Most mining from the Lynx and Wolverine zones will be complete, and barrier pillar recovery will commence. Production from the barrier pillar reserves prior to this year is limited to ramp development in ore. Barrier pillar recovery will continue until the partial year 2018 (120 operating days), when the mining reserve will be completely extracted.

The production forecast for 2007 through 2018 is provided in Table 1-1. Over the 12 years of production, the overall average mining rate, from startup through to closure, is 1380 t/d, with an average steady-state full production rate of 1441 t/d. The maximum mining for any given year is 1477 t/d, required for the year 2013.

Table 1-1: Annual Production Forecast

Year	Ore Mined (Kt)	Ore Milled (Kt)
2007	4,835	
2008	509,264	428,125
2009	529,688	456,250
2010	525,563	456,250
2011	528,325	456,250
2012	523,898	456,250
2013	538,973	456,250
2014	511,662	456,250
2015	514,815	456,250
2016	515,478	456,250
2017	367,428	304,167
2018	138,417	118,368
Total	**5,208,346**	**4,500,660**

1.3 Mill Operation

The processing facilities are designed to process 547,500 t/y of Wolverine deposit ore and to recover the contained copper, lead, zinc, gold and silver. The process will utilize conventional techniques in progressive particle size reductions, physical separation and concentration of the minerals of interest from gangue into concentrates at marketable grades. Particle size reductions will be achieved with crushing and grinding, while mineral separations will be achieved by dense media separation and flotation techniques. Processing will not involve chemical processes or alterations to the products. The low concentrations of reagents added during processing will largely be adsorbed on particle surfaces to facilitate the physical separation and will not generate chemical reactions.

An average of 1440 t/d of ROM ore will be processed through the crushing and DMS plants. The products from the DMS plant will include 190 t/d of non-sulphide 'float' (waste) which will be trucked to the tailings facility, and 1250 t/d of ore which will feed the concentrator. The process will produce an average of 46 t/d of copper concentrate, 26 t/d of lead concentrate, 239 t/d of zinc concentrate, and 939 t/d of tailings. Gold and silver will be recovered in the copper and lead concentrates.

Selected process streams will be sampled and analyzed in an on-stream analytical system for operations monitoring and control purposes. Any process spillages will be contained and collected in sumps within their respective areas, then pumped back into the process streams.

A water management system has been incorporated in the process to maximize water recycle and re-use. All water from the process facilities and underground will be collected in the tailings facility. The balance (94%) of the water will be reclaimed to the process water distribution system in the facilities.

1.3.1 Ore Haulage, Crushing and Storage

Run-of-mill (ROM) ore will be hauled by 40 t trucks from the underground mine to the dry crushing plant on the surface. The crushing plant has been designed for direct dump of the ore from the trucks. Depending on final mill design, there may be a temporary stockpile near the crusher where the ore is blended. This area will be compacted to minimize potential infiltration. The ROM ore will be crushed in two stages, with inter-stage screening from a top size of 450 mm to the 19 mm size required for the first bulk separation of gangue from ore in the DMS plant.

The combined crushed ore from the jaw and cone crusher will be conveyed to the vibrating screen. The screen oversize will feed the cone crusher. The cone crusher product, at 80% passing 19 mm, will be recycled to the vibrating screen via a conveyor. The crushing plant product is the screen undersize, which will drop onto a conveyor and be conveyed to a heated 1500 t capacity fine ore storage bin. The storage bin will provide the capacity necessary to keep the DMS plant running during short, unscheduled maintenance shutdowns of the crushing plant.

Following the DMS operation, multiple stages of particle size reduction and physical upgrading will be necessary to recover copper, lead and zinc minerals as high grade concentrates. Wet grinding mills will reduce particle size while a series of froth flotation cells will separate and upgrade minerals.

1.3.2 Metallurgical Programs and Flotation Circuit

The Wolverine Project has to-date had three major metallurgical development campaigns. The first was in 1997 with Amtel; then revisited in 2000 with Process Research Associates Ltd. and recently completed in 2005 with SGS Lakefield. The focus of each campaign was to develop a process flowsheet that would produce selective copper, lead, and zinc concentrates.

The 2005 Metallurgical Program employed the process flowsheet, grind and reagent scheme developed in 1997 at the Amtel Laboratory. The Wolverine and the Lynx orebodies do have similar mineral assemblages but the mineralogical evaluations indicated that the Lynx orebody had a slightly finer mineral grain size than the Wolverine orebody. The most recent laboratory development program initially tested the individual orebody composites and found that the process flowsheet and reagent scheme were similar so the two orebody composites were co-mingled (overall composite).

The laboratory batch flotation tests were used to evaluate the primary and regrind product sizes, reagent schemes and flowsheet process steps and thereby determine the optimum conditions/criteria to produce selective concentrates. When this was complete, a series of Locked Cycle flotation tests, typical of a continuous operation, were run to determine metal recoveries in the selective concentrates (copper concentrate, lead concentrate and zinc concentrate) and the multi-element content of each concentrate. Reagents will be added to the flotation circuit to modify the mineral particle surfaces and enhance their selective floatability. The reagents added are selectively adsorbed on each of the copper, lead and zinc minerals to produce their separation and recovery.

1.3.3 Reagents

An extrapolation of the reagent schemes and quantities used in the Locked-Cycle tests was the bases of the reagent scheme presented in Table 1-2.

Table 1-2: Projected Reagent Requirements

	LIME g/t	Na2S3O5 g/t	5100 g/t	Zn/CN g/t	Na2SO3 g/t	KEX g/t	MIBC g/t	CuSO4 g/t	pH
Primary Grind		2000							7.0
Prefloat							5		7.0
Cu RGHR	360		40				25		8.5
Cu REGRIND		250							7.0
Cu 1st CLNR	150						2.5		8.2
Cu 1st CLNR-SCAV			2.5						8.2
Cu 2nd CLNR		50							7.9
Cu 3rd CLNR		25							7.9
Pb RGHR				150	1250	30			8.5
Pb REGRIND				150	200	5			8.1
Pb 1st CLNR									8.1
Pb 1st CLNR-SCAV						4			8.1
Pb 2nd CLNR					50				8.1
Zn COND	900		60					500	10.0
Zn RGHR						25	2.5		10.0
Zn REGRIND	1000		5					200	11.3
Zn 1st CLNR									11.3
Zn 1st CLNR-SCAV			12.5				2.5		11.6
Zn 2nd CLNR	155								11.6
Zn 3rd CLNR	180						2.5		11.6
Zn 4th CLNR	180						2.5		11.6
Totals	**2925**	**2325**	**120**	**300**	**1500**	**64**	**20**	**700**	

The reagents required for selective copper flotation will consist of lime, sodium metabisulphite, Aero 5100 (dialkyl thionocarbamate), and MIBC. Copper flotation tailings will be pumped to the lead flotation conditioning tank. Lead flotation reagents will include sodium sulphite, potassium ethyl xanthate (KEX) and zinc cyanide (a complex that will be made on-site by mixing zinc sulphate with sodium cyanide solution). It is noted that there will be no free cyanide in the flotation slurry. The zinc cyanide complex added is not expected to break down in the alkaline conditions in the flotation circuit. The actual cyanide added will be equivalent to approximately 8 ppm in the flotation solution. Any cyanide complex remaining in the final tailings is expected to be insignificant.

The zinc cyanide complex will be added to depress pyrite and facilitate the upgrading of lead concentrate. Lead flotation tailings will be pumped to the first of three zinc conditioning tanks operating in series prior to zinc flotation. Zinc flotation reagents will include lime, sodium sulfite, KEX and zinc cyanide.

The products of the concentrator will be 0.8 t/h of pre-flotation concentrate, 2.1 t/h of copper concentrate, 1.2 t/h of lead concentrate, 10.8 t/h of zinc concentrate, and 41.7 t/h of final concentrator tailings. The entire final flotation tailings stream will be pumped either to the paste backfill plant when it is operating or to the tailings pond when paste backfill is not required by underground.

1.3.4 Reagent Preparation

Freshwater will dilute powdered reagents to facilitate their addition and control using metering pumps. Liquid reagents will be metered to process as-is. All reagents will be prepared in a separate, self-contained area within the concentrator building, then delivered by individual metering pumps to the addition points.

Forty tonne trucks will deliver lime to site in powder form and be pneumatically off-loaded into the lime silo. It will be mixed in fresh water to produce a 20% milk of lime slurry to enhance its utilization as a pH modifier. The slurry will be pumped continuously in a return loop around the flotation area. Valves controlled by pH controllers will add the slurry in pulses to maintain pre-set pHs in the flotation cells.

Sodium metabisulphite, sodium sulphite, zinc sulphate, sodium cyanide, potassium ethyl xanthate (KEX) and copper sulphate will be delivered in one tonne bags and stored in a dry area near the make-up systems. Each reagent make-up system will comprise a bag handling system, agitated mix tank, holding tank and metering pumps. Each reagent will be dissolved batch-wise in freshwater in the mix tank to approximately 10% concentration then transferred to the holding tank, based on a level controller in the holding tank. Metering pumps will deliver the reagents from the holding tanks to the addition points. Each mixing tank will be vented to atmosphere outside the plant to remove the minor amounts of dust generated during bag dumping.

Methyl isobutyl carbinol (MIBC) and Aero 5100 will be delivered as a liquid in approximately 200 kg drums and transferred into storage tanks. Metering pumps will deliver the as-received reagents to their addition points in the flotation circuit.

Zinc cyanide for the process will be prepared at site by mixing zinc sulphate powder and sodium cyanide powder in water, in a prescribed ratio to a 10% concentration. Lime will be added to maintain solution alkalinity. The solution will then be transferred from the mix tank to the holding tank and metered to the addition points.

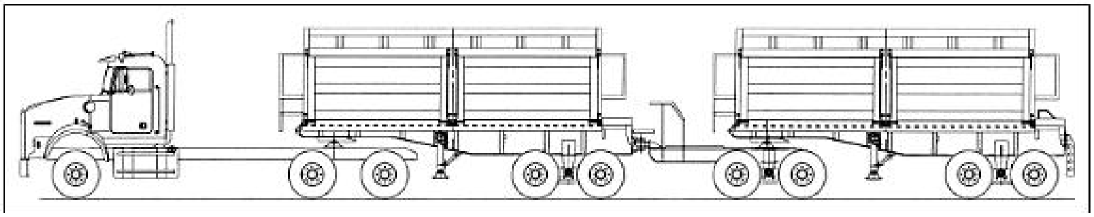
Spillages of each reagent will be contained within its own area in an in-ground sump, and then pumped back into the holding or storage tank.

1.4 Concentrate Haulage

Concentrates will be transported from the industrial complex to the Robert Campbell Highway (Highway 4) via the proposed 24 km long mine access road. The haul trucks will then proceed to the Port of Stewart for onward shipping to Asian smelters. Approximately 10 round trips per day (10 full and 10 empty haul trucks) will be required based on the proposed production rate.

YZC will use transport trucks with Super-B train trailers to transport concentrates to the Port of Stewart. The covered containers will prevent the loss of product and the potential for metal contamination along haulage corridors. Figure 1-1 shows an example of the side-dump concentrate haul truck that will be used.

Figure 1-1: Side-Dump Concentrate Haul Truck (Courtesy of Arrow Transportations Systems)



1.5 Power Plant

The site electrical power requirements will be met by a modular powerhouse comprised of seven Caterpillar 3516 diesel gensets, prime rated at 1500 kW each. These gensets are well proven for remote northern power generation in both mining and utility applications. The diesel gensets will be furnished with heat recovery systems to service the site heating load, as well as conventional radiators for complete heat rejection, when required.

The seven units provide N+2 redundancy to ensure high availability and margin for load growth. The gensets are segregated between 600 and 4160 V busses according to the division of plant load. A single 2000 kVA, 4160/600 V dry-type transformer allows power transfer between the two busses. This configuration minimizes site distribution transformer requirements and has the added benefit of yielding managable fault levels on each of the 600 and 4160 V busses, thereby minimizing switchgear costs. The main 600 and 4160 V switchboards will be located in the modular powerhouse with 1 and 5 kV feeder cables emanating to the load centres via the utilidors.

The modular powerhouse is be located in close proximity to the main process and secondary buildings (Drawing A0-C-006). This allows the bulk of the power distribution to these buildings to be at the 600 V utilization voltage. The 600 V load in the main process plant and secondary buildings is served by single-ended Motor Control Centres (MCCs). The load is generally segregated by a process and/or functional area. In turn, these MCCs are served by six Power Distribution Centres (PDCs), which distribute power from the incoming 600 V feeders to the MCCs. This configuration facilitates protection coordination and isolation of MCCs for maintenance purposes. Most of the 600 V PDCs and MCCs will be housed in a pre-fabricated electrical room adjacent to the main process building, with subsets in the powerhouse and service building.

As noted above, power distribution to the main process and service buildings will be by 1 and 5 kV feeder cables from the main switchboard 600 and 4160 V busses. Two 5 kV feeder cables will also be provided to the mine portal and surface ventilation fans from the 4160 V MCC. The bare conductor overhead line will transition from 5 kV cable just outside of the main industrial site. Site loads remote from the powerhouse include the camp, water treatment, landfill and tailings facility.

1.6 Fuel Storage

Diesel fuel requirements for the power generators, underground and surface mobile equipment will be supplied from diesel fuel storage tanks located near the service building and the generators. Facilities will be provided for metering at the tank farm. Tanks will be provided for separate grades of fuel for power generation and for mobile equipment.

Approximately eight 45,000 L capacity B-train tanker trucks per week will be required to supply the power plant and surface mobile equipment. Due to road conditions during the winter months, two 151 m^3 storage tanks will be required to provide weekly storage capacity. The fuel station/storage area is located between the mill and the truckshop/offices (Drawing A0-C-006). The diesel storage and dispensing tanks will be erected within a lined containment area sized to contain 110 % capacity of the tanks.

The dispensing station will be provided with a smaller fuel tank with capacity less than 50,000 L in accordance with requirements of National Fire Code of Canada. The estimated maximum power plant consumption rate is 48,000 L/day. The surface mobile equipment has a consumption rate of approximately 1552 L/day.

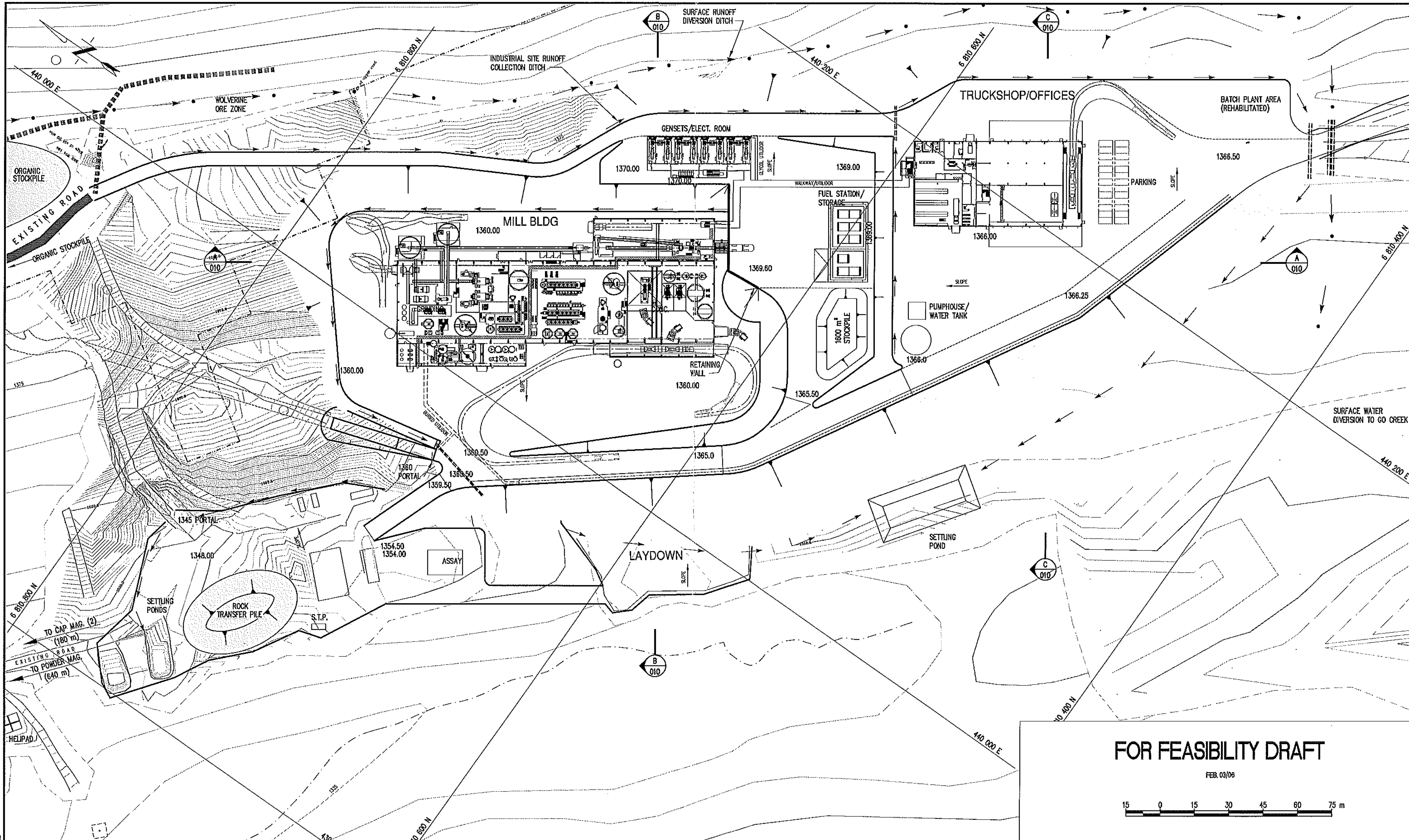
Fuel for the diesel generators will be pumped to day tanks built into the floor of each generator module.

The underground mine mobile equipment requires Low Sulfur No. 2 Diesel to meet current emission standards for underground vehicles. The fuel from B-train tanker truck will be transferred to the tank and will be pumped to the fuel dispensing station for the underground equipment. The underground mobile equipment has a consumption rate of approximately 3450 L/day.

Lubricants will be delivered to the site in drums where they will be stored in a secure area. The lubricants will be distributed to hose reels in the truckshop service bay with barrel pumps.

There are no plans to store and dispense gasoline at the project.

Drawings



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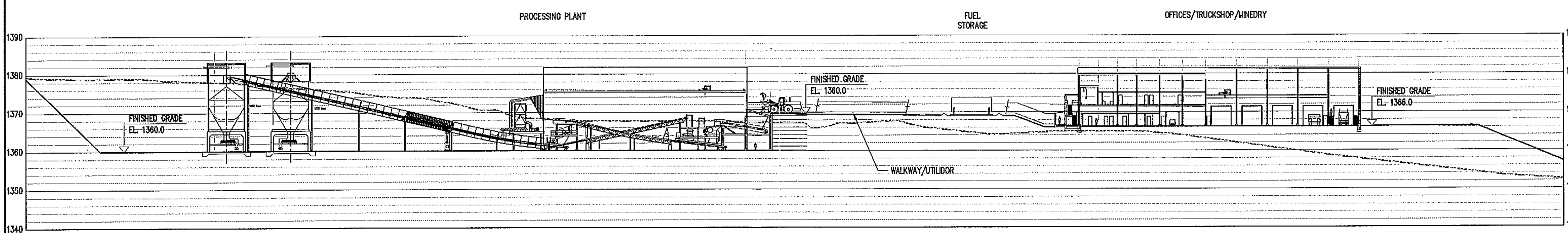
WOLVERINE PROJECT

INDUSTRIAL COMPLEX AREA LAYOUT



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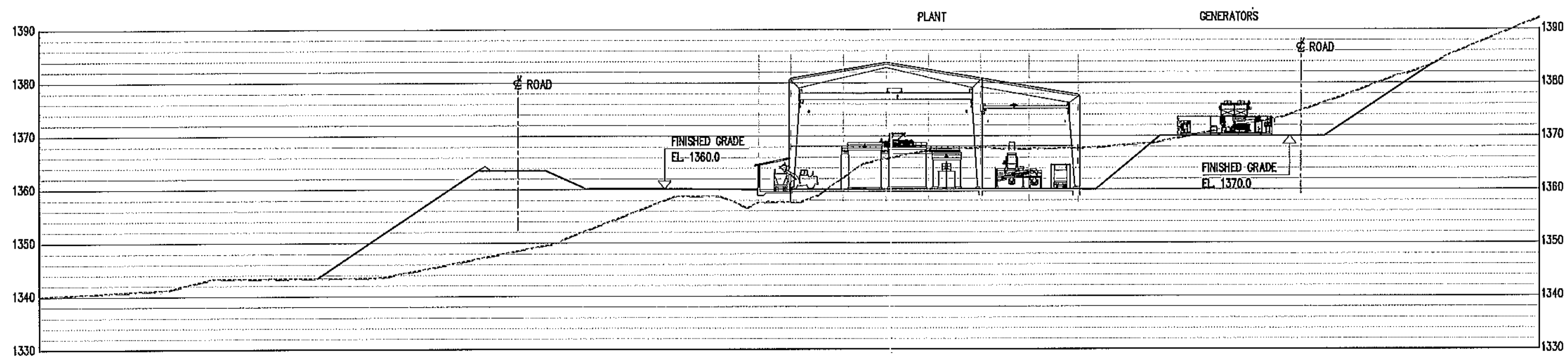

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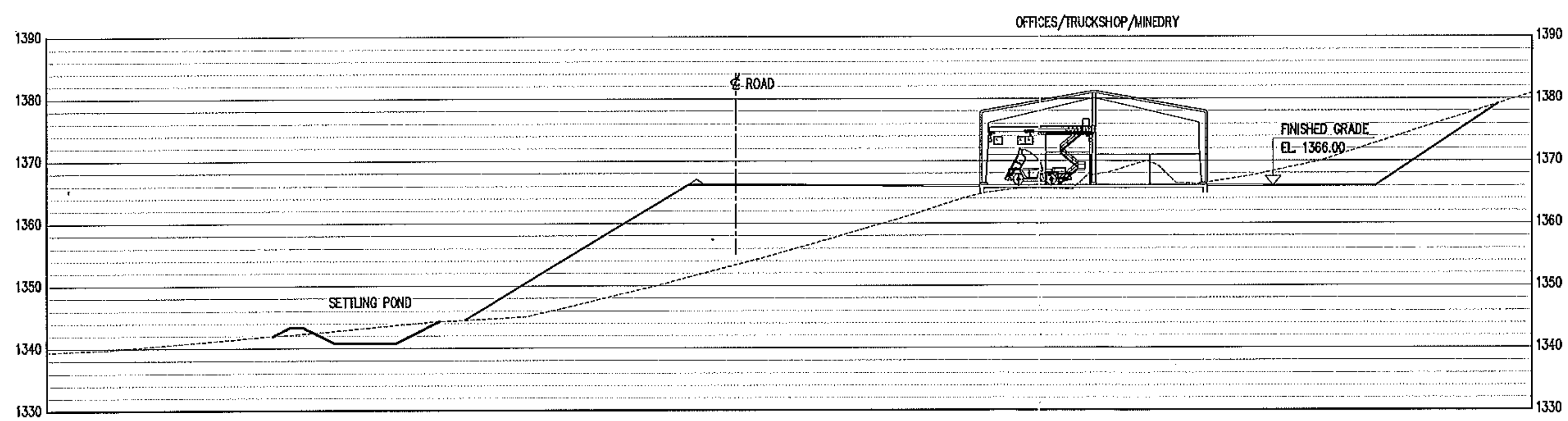

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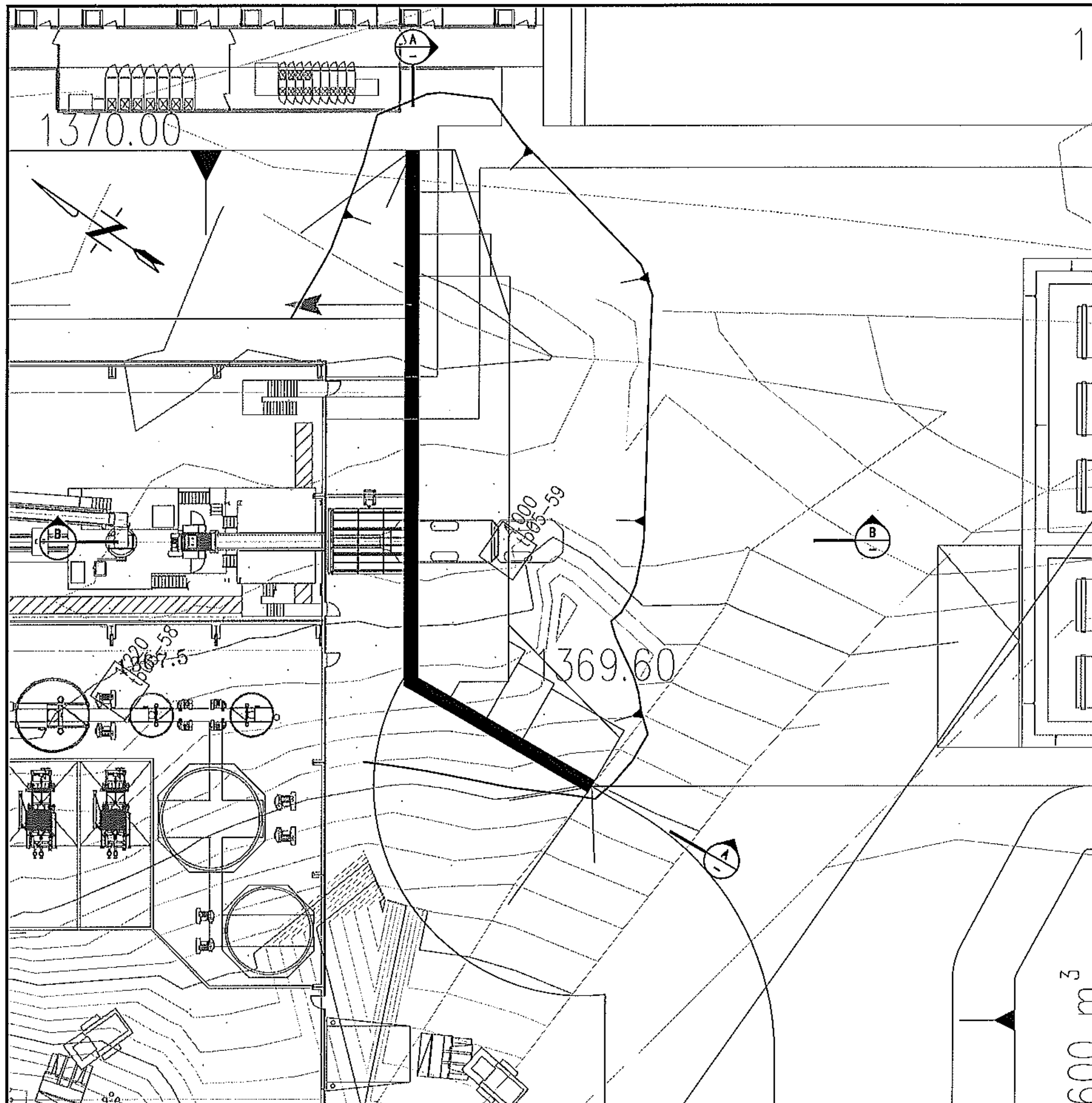
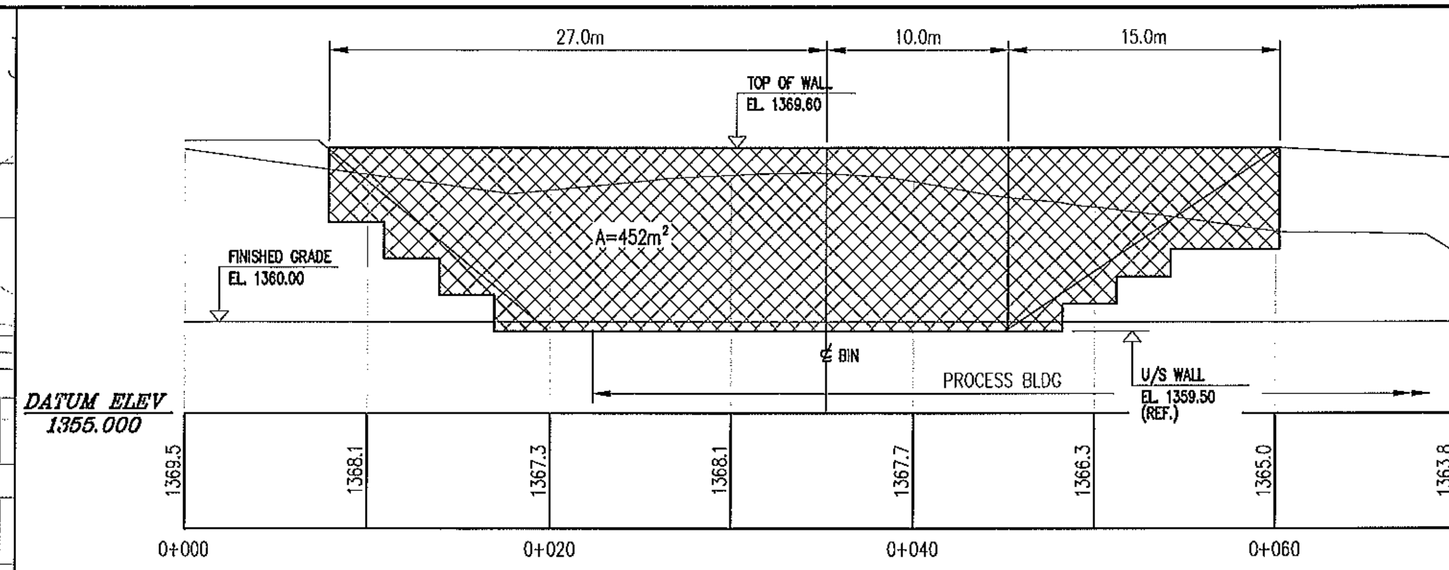
WOLVERINE PROJECT

INDUSTRIAL COMPLEX SECTIONS





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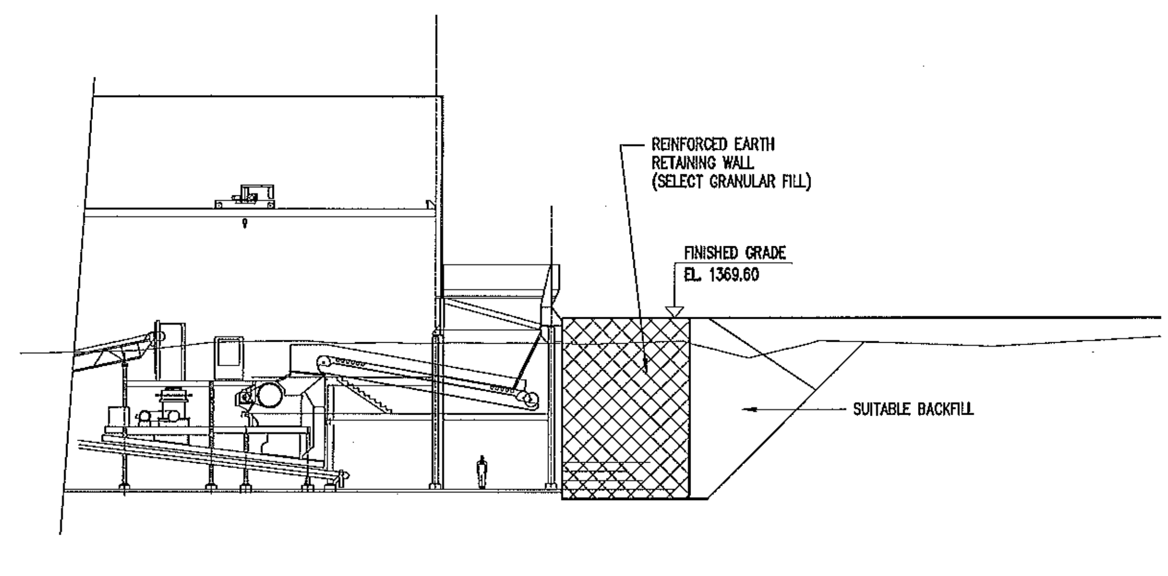

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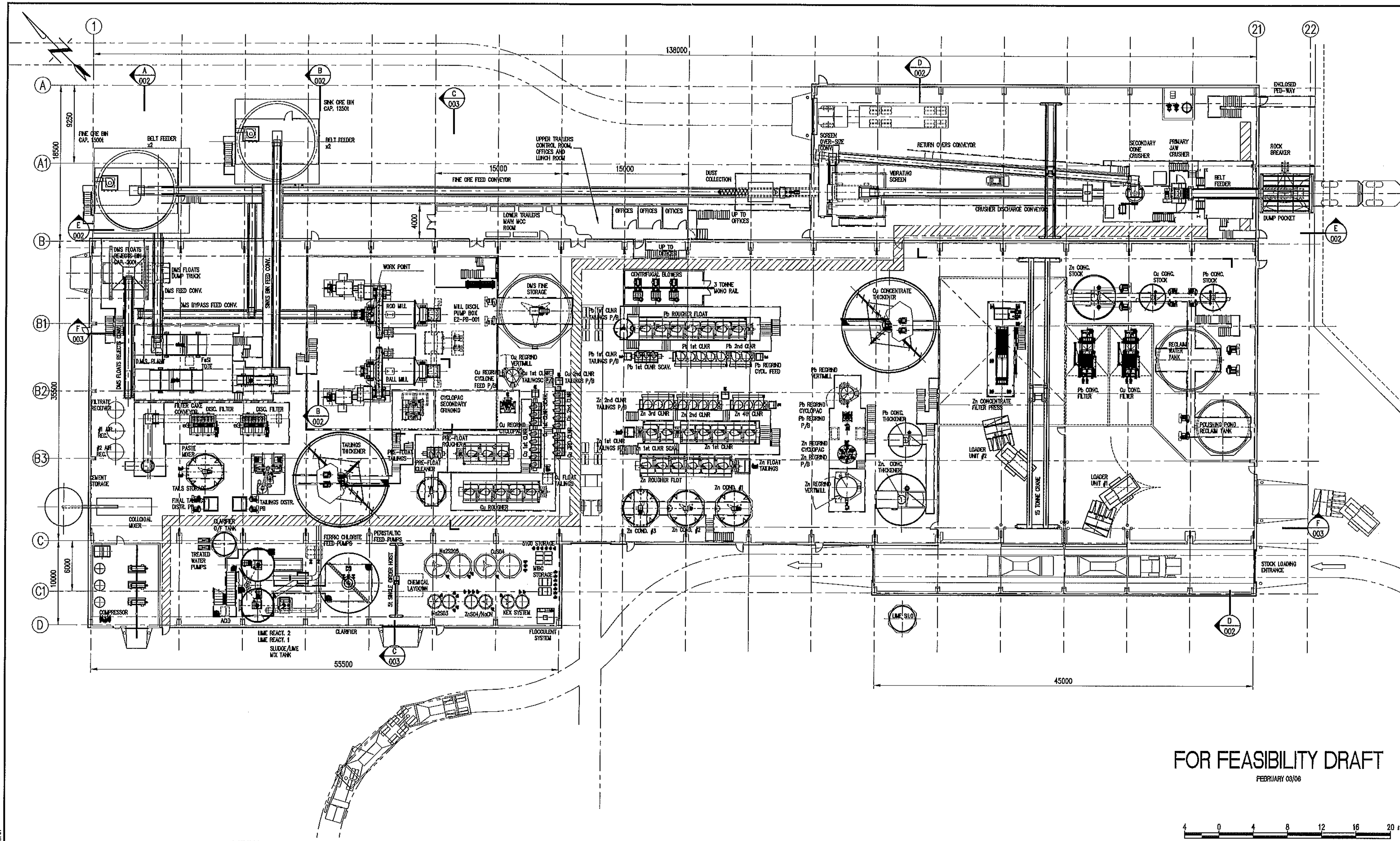
WOLVERINE PROJECT

RETAINAING WALL
PLAN AND SECTIONS



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WOLVERINE PROJECT

WOLVERINE PLANT SITE GENERAL ARRANGEMENT PLAN VIEW

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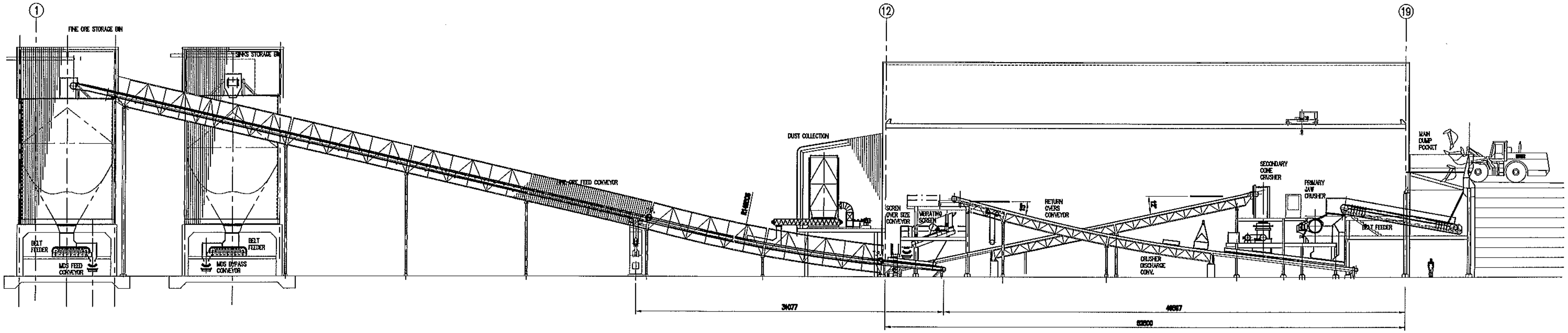

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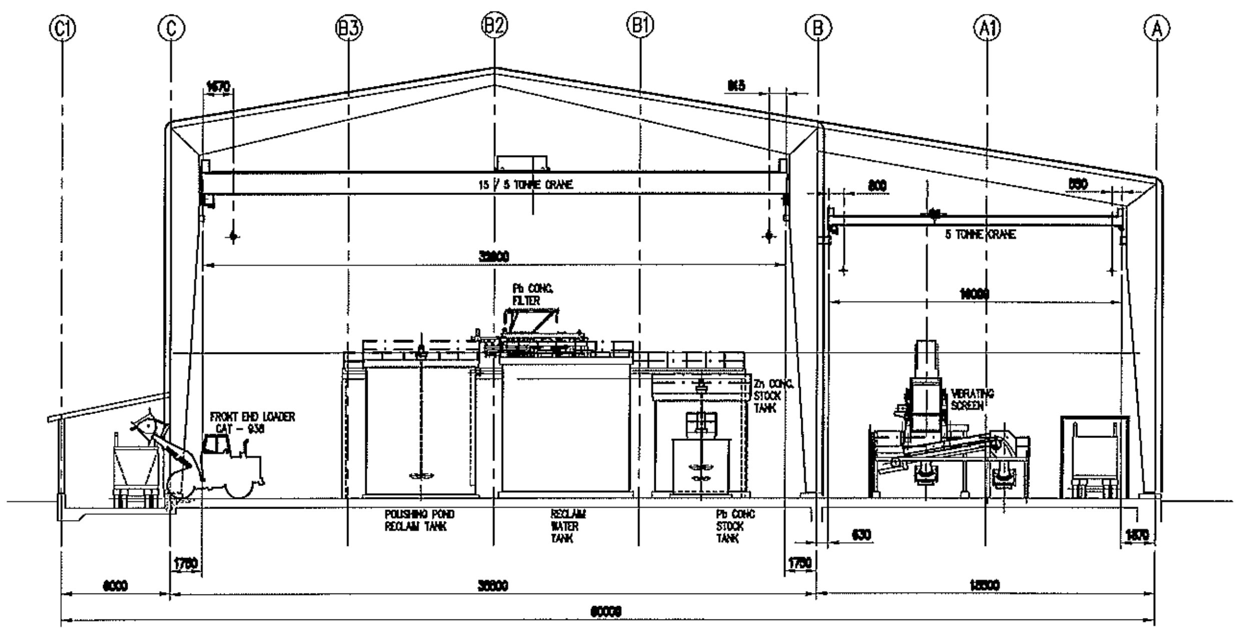

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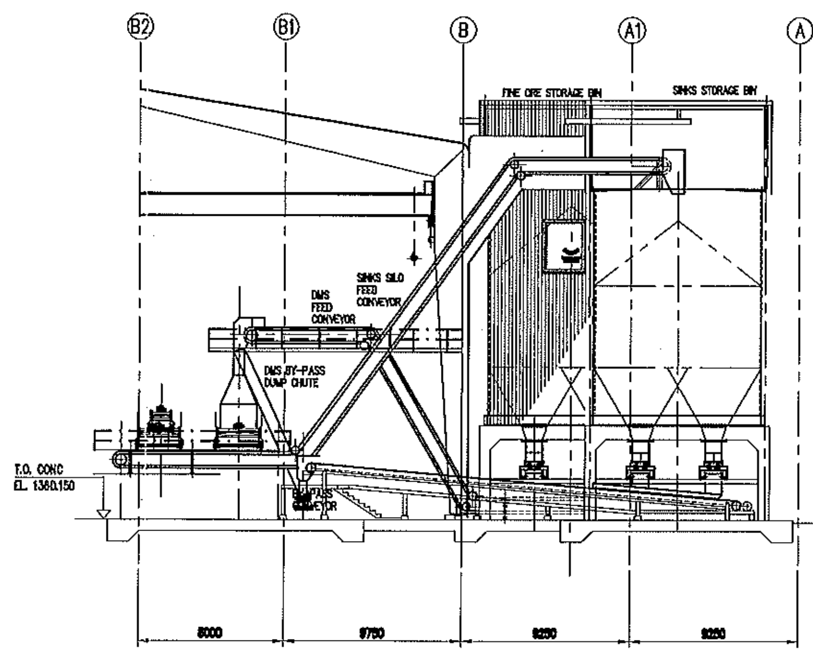

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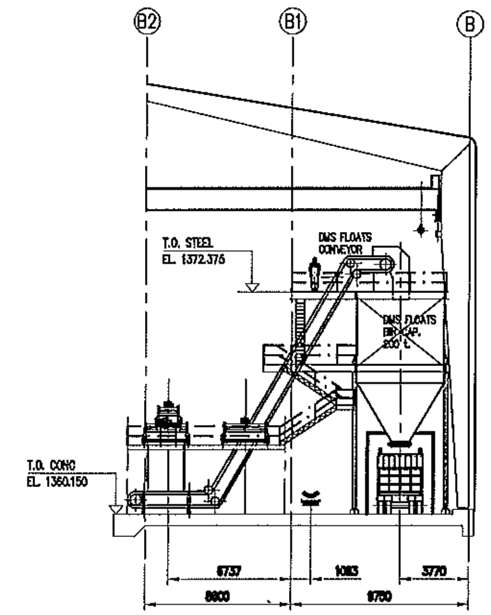

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WOLVERINE PROJECT

WOLVERINE PLANT SITE
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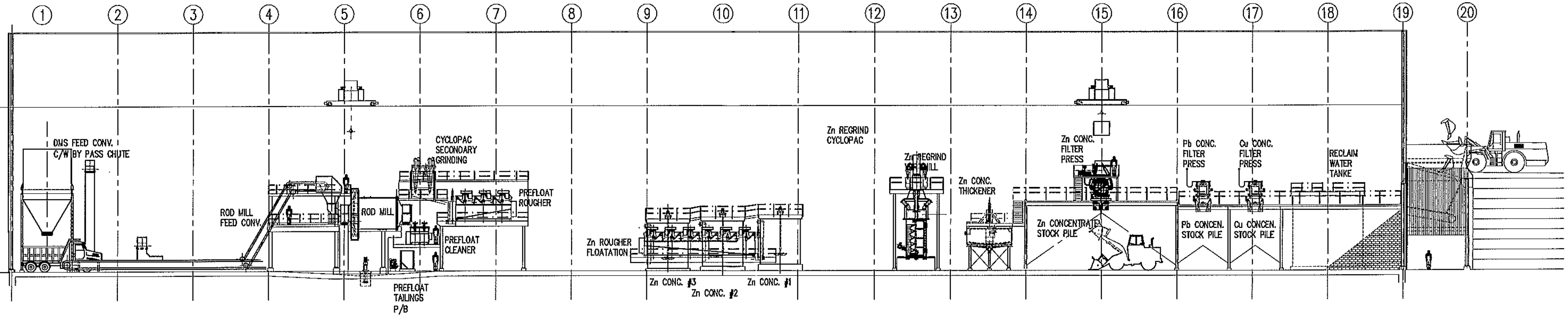
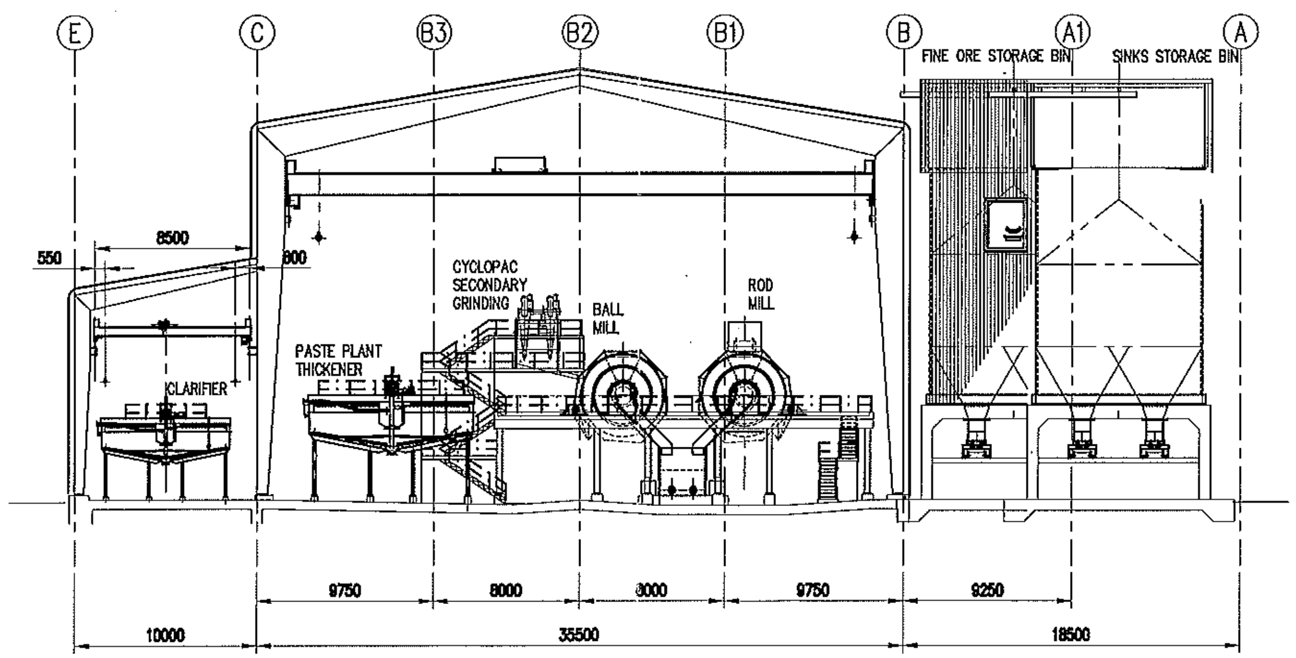


SECTION F / 001



SECTION C / 001

FOR FEASIBILITY DRAFT

FEBRUARY 03/06

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2006/01/10 09:38

DWG. NO.	REFERENCE DRAWINGS
F1-G-002	PLANT GENERAL ARRANGEMENT - SECTIONS
F1-G-001	PLANT GENERAL ARRANGEMENT - PLAN

PROJECT PROCESS CIVIL MECH. STRUCT. PIPING SERVICES ELECT. INSTR.

NO	DESCRIPTION	BY	DATE
A	ISSUED WITH FEASIBILITY - DRAFT	GZ	01.12.06

ISSUE/REVISIONS

PROJECT PROCESS CIVIL MECH. STRUCT. PIPING SERVICES ELECT. INSTR.

NO	DESCRIPTION	BY	DATE

ISSUE/REVISIONS

SECTION:		
SCALE:	1:200	DATE
DESIGN. BY	G. Zwiep	11/24/05
DRAWN BY:	G. Zwiep	11/24/05
CHECK. BY	G. Martin	
APP. BY:	J. Shillabeer	

FILENAME:	PROJECT NUMBER	DRAWING NUMBER	REV.
F0G003.DWG	319065	F1-G-003	A

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Yukon

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WOLVERINE PROJECT

WOLVERINE PLANT SITE
GENERAL ARRANGEMENT
CROSS SECTIONS